

## Technical Article

# Buffering of Acidic Mine Lakes: The Relevance of Surface Exchange and Solid-Bound Sulphate

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**Abstract.** Buffering mechanisms in an acidic mine lake in Lusatia, Germany were investigated. The titration curve has four sections with different buffering mechanisms: (1) buffering by free hydrogen ions and hydrogen sulphate ( $\text{pH} = 2.55\text{--}2.9$ ), (2) buffering by Fe with bound  $\text{SO}_4$  ( $\text{pH} = 2.9\text{--}4.3$ ), (3) buffering by Al with bound  $\text{SO}_4$  ( $\text{pH} = 4.3\text{--}5.5$ ), and (4) buffering by surface exchange of  $\text{SO}_4$  and basic cations ( $\text{pH} > 5.5$ ). Three different phase models were applied to simulate the titration curve: (1) an iron and aluminium hydroxide model; (2) an iron and aluminium hydroxysulphate model; and (3) an iron hydroxide model with surface exchange for  $\text{SO}_4$ , Ca, and Mg, coupled with an aluminium hydroxysulphate model. The uncertainty of model input parameters was accounted for in a sensitivity analysis. Only the third model, which considers surface exchange, was able to adequately reproduce the measured titration curve.

**Key words:** acidic mining lakes; Lusatia; pH buffering; PHREEQC modelling; surface complexation; titration

## Introduction

Lakes that develop in lignite open pits after mining due to natural groundwater rebound are often characterised by a low pH and high concentrations of Fe, Al, and  $\text{SO}_4$  due to acid input from mine waste and adjacent groundwater bodies (Schnoor et al. 1997; Grünewald 1999). Three possible remediation strategies for these lakes are: flooding with alkalinity-buffered surface waters from regional rivers; chemical treatment with alkaline substances such as limestone, lime, or sodium hydroxide; and the promotion of biological reductive processes (Klapper et al. 1998; Skousen et al. 1998; Uhlmann et al. 2001; Totsche and Steinberg 2003). The objective of all of these strategies is the long-term decrease and elimination of acidity in the mine lakes, thereby increasing the pH to circumneutral values.

In the extremely acidic mining lakes in Lusatia, north-eastern Germany, acidity [titrated to pH 4.3 (hereafter referred to as base neutralization capacity or  $\text{BNC}_{4.3}$ )] values reach up to  $10\text{--}15\text{ mmol L}^{-1}$  and, in extreme cases, up to  $30\text{ mmol L}^{-1}$ , due to high concentrations of dissolved ferric iron and aluminium

(Nixdorf et al. 2001; Nixdorf et al. 2003). These lakes are characterised by pH values between 2 and 4 and are mainly Fe buffered (Klapper et al. 1996; Geller et al. 1998). A few lakes are aluminum buffered, with pH values in the range of 4 to 5, similar to lakes affected by acid rain (Ulrich 1981).

Buffering characteristics can be described by titration curves. These curves relate pH to acidity and have previously been used in the context of acidic mining lakes (Fyson and Kalin 2000; Totsche et al. 2002). In this study, the titration curve of acidic water from a mine lake in Lusatia was investigated in detail. The objective was to obtain a detailed understanding of buffering mechanisms relevant to lake water neutralisation as well as a quantitative description by hydrochemical modelling. Phases precipitated during titration were analysed by standard analytical methods as well as mineralogical structure analyses (Totsche et al., submitted).

## Material and Methods

The study was performed on water samples from the epilimnion of the Plessa 111 mine lake in Lusatia, north-eastern Germany. The lake developed by natural groundwater rebound after mining ended in 1956. The lake is  $110,000\text{ m}^2$  in area, with a maximum depth of about 10 m. It has a pH of 2.55, a  $\text{BNC}_{4.3}$  of  $\approx 10\text{ mmol L}^{-1}$  (and a  $\text{BNC}_{8.2}$  of  $15.5\text{ mmol L}^{-1}$ ), and high dissolved iron (ca.  $150\text{ mg L}^{-1}$ ), aluminium (ca.  $30\text{ mg L}^{-1}$ ), and sulphate (ca.  $1300\text{ mg L}^{-1}$ ), which is typical for acid mining lakes in Lusatia (Nixdorf et al. 2001).

The acidic water was titrated with 0.1 N NaOH using an automatic titrator and continuous stirring. Titrations were carried out continuously and discontinuously. During discontinuous titrations, a defined amount of base was added at every step. After adding the base, mixing was stopped and precipitates were collected in sediment traps and removed.

Water samples were filtered with a  $0.45\text{ }\mu\text{m}$  sodium acetate filter by compressed air. Water samples were analysed for dissolved Fe, Al, Mn, Ca, and Mg by atomic absorption spectrometry (AAS 3300, Perkin Elmer), for Na and K by atomic emission spectrometry

(AAS 3300, Perkin Elmer), and for  $\text{SO}_4$  and  $\text{Cl}$  by a Shimadzu ion chromatography system.  $\text{Fe}^{2+}$  was analysed photometrically (Photometer UV 2101, Shimadzu) using the 1,10-phenanthroline method. Precipitates were dried for about 40 hours at  $105^\circ\text{C}$  and ground with mortar and pestle before analysis. Solid phase samples were analysed for Fe, Al, Mn, Ca, Mg, Na, K, and total S.

The titration curve was simulated using the geochemical simulator PHREEQC (Parkhurst and Appelo 1999). Three different equilibrium phase models were applied. In the simplest model, the precipitating phases were iron and aluminium hydroxide, and manganese oxide. In the second model, iron and aluminium hydroxysulphate took the place of the hydroxide phases. The third model accounted for surface complexation. For Fe, a hydroxide model with sorptive attributes, which considers the pH-dependent protonation and deprotonation of hydroxyl groups as well as adsorption and desorption of  $\text{SO}_4$ , Ca, and Mg, was applied. Thermodynamic constants for surface complexation on hydrous ferric oxides were taken from Dzombak and Morel (1990). For Al, the hydroxysulphate model was applied, as in phase model (2), as thermodynamic constants for surface complexation were not available in the PHREEQC data set. For Mn, the oxide model was applied, as in phase models (1) and (2).

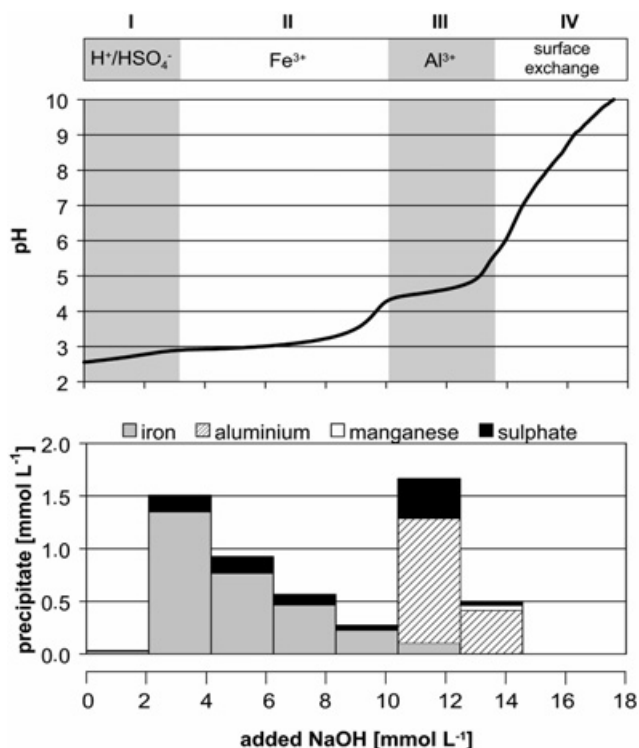
The models all assume a constant partial pressure for oxygen, guaranteeing oxic conditions in the model as in the experiment.  $\text{CO}_2$  gas exchange was not accounted for in the standard model, but its effects were investigated in a special consideration.

## Results and Discussion

### Experiments

Titration experiments were performed six times using the same water sample. Titration curves were highly congruent (data not shown). On the whole, about 100 titration curves were recorded, all based on lake 111 water samples. The curves differ only slightly depending on the pH, and the Fe and the Al concentrations. The time span of the continuous titration was  $\approx 15$  hours. However, we found no significant time dependency in the titration curves using other time intervals between hours and days.

The detectable inorganic carbon (TIC) concentration in the mine water was below  $0.5 \text{ mg L}^{-1}$ . This is in accordance with TIC measurements in most of the pit lakes in Lusatia, which show TIC concentrations in equilibrium with the atmospheric partial pressure ( $\approx 10^{-3.5}$  bars) of approx.  $0.2 - 0.3 \text{ mg L}^{-1}$ .



**Figure 1.** Measured titration curve of the acidic lake water and composition of the precipitates; the grey shades denote the different buffering sections

During the titration experiments, the redox potential was measured continuously. The initial measurements ( $E_h \approx +790 \text{ mV}$ ) show oxic conditions and the predominance of  $\text{Fe}^{3+}$ . The detectable  $\text{Fe}^{2+}$  concentration in the lake water was below  $0.05 \text{ mg L}^{-1}$ . The measured titration curve of the acidic lake water is shown in Figure 1. Additionally, the main constituents of the precipitates, obtained in seven steps, are depicted.

The titration curve can be divided into four sections. In section I ( $0.0 - 3.0 \text{ mmol L}^{-1}$  NaOH added), the pH increased continuously, from 2.55 to 2.9. Precipitation was negligible. In general, a pH rise from 2.55 to 2.9 is associated with a decrease of the free hydrogen ion concentration of about  $1.5 \text{ mmol L}^{-1}$ . Thus, about  $1.5 \text{ mmol L}^{-1}$  of the  $3.0 \text{ mmol L}^{-1}$  base added in this section was solely consumed by the neutralisation of hydrogen ions. The remaining base added was used for the deprotonation of hydrogen sulphate as well as for the homogeneous hydrolysis of iron.

In section II ( $3.0 - 10.0 \text{ mmol L}^{-1}$  NaOH added), the pH was nearly constant at  $\text{pH} \approx 3$ . An orange iron hydroxysulphate, with a mean Fe/S molar ratio of 5.6:1, precipitated. The Fe/S molar ratio is in the range of that typically found for schwertmannite (Bigham et al. 1990). Mineralogical analyses (infrared and x-ray diffraction) confirmed that schwertmannite was present (Totsche et al., submitted). After the plateau, there was a short and weakly buffered transitional

section in which the pH rose to 4.3. Section II was dominated by Fe buffering, as dissolved  $\text{Fe}^{3+}$  in the acidic water hydrolysed and precipitated. The process releases hydrogen ions, delaying a further rise of pH.

In section III (10.0 – 13.5 mmol L<sup>-1</sup> NaOH added), a second plateau occurred (pH = 4.3 to 5.5) due to Al buffering. A white sediment with an Al/S molar ratio of 2.7:1 precipitated. Based on the sulphur content, the precipitate was aluminium hydroxysulphate. Since the precipitate was x-ray amorphous, further mineralogical analyses was not possible. The stoichiometry, however, is in the range of known aluminium hydroxysulphate minerals, such as basaluminite, with an Al/S molar ratio of 4:1.

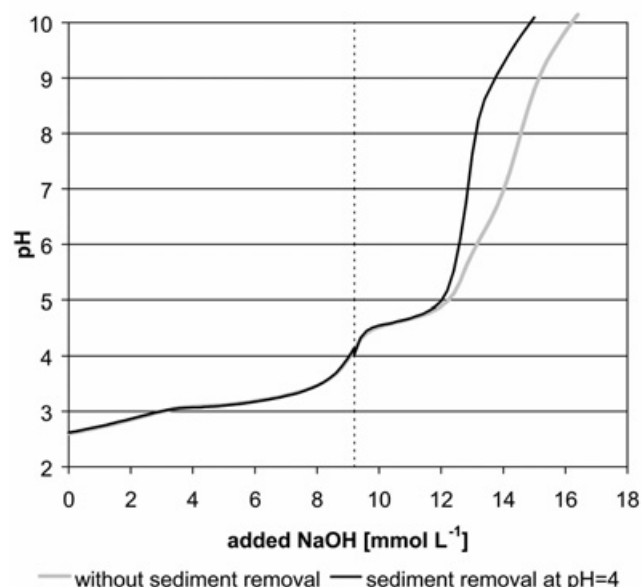
In section IV (> 13.5 mmol L<sup>-1</sup> NaOH added), the pH increased relatively linearly, starting at pH = 5.5. Precipitates were minor and mainly consisted of manganese oxides. The buffering mechanism in this section was coupled to the solid phase; if precipitates were removed, the pH increase was steeper, i.e. less base had to be added, and buffering was much less effective. Figure 2 depicts the curve of continuous titration compared to a titration curve with separation of precipitates at pH = 4 after the addition of 9.2 mmol L<sup>-1</sup> NaOH. The steep increase of the titration curve after the separation of precipitates (at  $\approx 12$  mmol L<sup>-1</sup> NaOH) indicates the decisive influence that surface effects have on buffering. Investigating the alteration of precipitate composition between pH = 5.0 and 8.5 gives further indications of the buffering mechanism (Figure 3). The acidic precipitate at pH = 5 contained considerable amounts of  $\text{SO}_4$ , but no Ca and Mg. In contrast, the alkaline precipitate at pH = 8.5 clearly contained Ca and Mg and distinctly less  $\text{SO}_4$ . Sulphate release as well as adsorption of Ca and Mg both release hydrogen ions and could cause the section IV buffering.

## Modelling

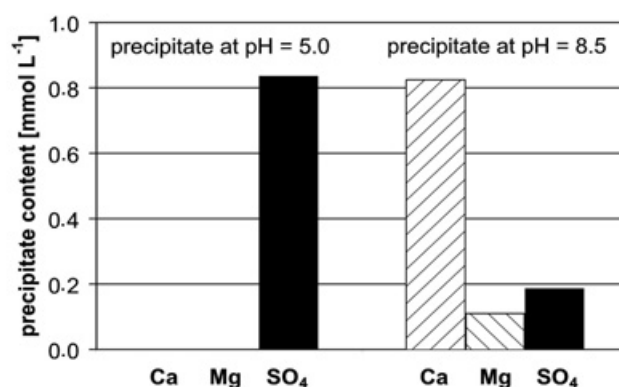
Modelling was used to investigate if these processes could quantitatively explain the observed buffering. The following input parameters were required:

- Composition of the initial acidic solution
- Fe and Al hydroxysulphate stoichiometries
- Solubility products of the precipitating phases
- Surface complexation reactions with their thermodynamic data
- number of exchange sites on the hydrous ferric surface

The model parameterisation for the Plessa 111 mining lake is summarised in Table 1. Ion activities for the lake water composition were calculated with PHREEQC, according to the Debye-Hückel model.



**Figure 2.** Comparison of titration curves of the continuous titration and of the titration with sediment removal after addition of 9.2 mmol L<sup>-1</sup> NaOH.



**Figure 3.** The amounts of calcium, magnesium, and sulphate in the precipitating sediment during the titration up to pH = 5 and up to pH = 8.5.

The solubility products of iron hydroxide or schwertmannite, respectively, and aluminium hydroxysulphate were fitted to the buffering plateaus of the titration curve. Iron and aluminium hydroxysulphate stoichiometries were calculated from measured Fe/S and Al/S molar ratios in the precipitates. The exchange capacity of precipitating iron hydroxides was adjusted in such a way that using the intrinsic thermodynamic dissociation constants for iron hydroxide as well as the complexation constants for  $\text{SO}_4$  given in PHREEQC led to a good reproduction of measured surface-complexed  $\text{SO}_4$  contents. In general, there was a good agreement between these values and literature values (Table 2). For iron hydroxide, a  $\text{pK}_{\text{sp}}$  of 4.0 was determined, which is in line with a  $\text{pK}_{\text{sp}}$  of 4.9 for amorphous ferrihydrite. For iron oxyhydroxysulphate, the derived  $\text{pK}_{\text{sp}}$  was 21.0, which is similar to the  $\text{pK}_{\text{sp}}$  for

schwertmannite,  $18 \pm 2.5$ . The determined  $pK_{sp}$  for aluminium hydroxide is 9.0, and thus in between the values for amorphous aluminium hydroxide (10.8) and gibbsite (8.1). Finally, for aluminium hydroxy-sulphate, a  $pK_{sp}$  of 5.0 was derived, which is close to the  $pK_{sp}$  of 5.7 for basaluminite. Equations and thermodynamic data for surface exchange were taken from Dzombak and Morel (1990), as implemented in the WATEQ4F.dat data base of PHREEQC, with minor modifications for Ca and Mg (Table 1C).

### Sensitivity Analysis

The inaccuracy of model input parameters was accounted for in a sensitivity analysis. The most sensitive parameters for the shape of the titration curve are the concentrations of free hydrogen ions, which is characterised by the pH of the initial

**Table 1.** Model parameterisation including precipitation and surface exchange reactions

#### A. Initial Solution

Parameter	Value
pH	2.55
Sodium	0.31 mmol L <sup>-1</sup>
Potassium	0.08 mmol L <sup>-1</sup>
Magnesium	1.10 mmol L <sup>-1</sup>
Calcium	4.64 mmol L <sup>-1</sup>
Iron	2.68 mmol L <sup>-1</sup>
Aluminium	1.05 mmol L <sup>-1</sup>
Manganese	0.06 mmol L <sup>-1</sup>
Sulphate	13.63 mmol L <sup>-1</sup>
Chloride	0.25 mmol L <sup>-1</sup>

#### B. Phase Models

Model	Precipitation reaction	$pK_{sp}$
hydroxide model	$Fe^{3+} + 3 H_2O \rightarrow Fe(OH)_3 + 3 H^+$	4
	$Al^{3+} + 3 H_2O \rightarrow Al(OH)_3 + 3 H^+$	9
hydroxysulphate model	$8 Fe^{3+} + 1.44 SO_4^{2-} + 13.12 H_2O \rightarrow Fe_8O_8(OH)_{5.12}(SO_4)_{1.44} + 21.12 H^+$	21
	$Al^{3+} + 0.37 SO_4^{2-} + 2.26 H_2O \rightarrow Al(OH)_{2.26}(SO_4)_{0.37} + 2.26 H^+$	5
surface complexation model	$Fe^{3+} + 3 H_2O \rightarrow Fe(OH)_3 + 3 H^+$	4
	$Al^{3+} + 0.37 SO_4^{2-} + 2.26 H_2O \rightarrow Al(OH)_{2.26}(SO_4)_{0.37} + 2.26 H^+$	5
all models	$Mn^{2+} + 2 H_2O \rightarrow MnO_2 + 4 H^+ + 2 e^-$	-43.6

#### C. Surface Exchange Processes (Dzombak and Morel 1990)

	Reaction	pK
protonation / deprotonation	$Hfo-wOH + H^+ \rightarrow Hfo-wOH_2^+$	-7.29
	$Hfo-wOH \rightarrow Hfo-wO^- + H^+$	8.93
sulphate	$Hfo-wOH + SO_4^{2-} + H^+ \rightarrow Hfo-wSO_4^- + H_2O$	-7.78
	$Hfo-wOH + SO_4^{2-} \rightarrow Hfo-wOHSO_4^{2-}$	-0.79
base cations <sup>1</sup>	$Hfo-wOH + Ca^{2+} \rightarrow Hfo-wOCa^+ + H^+$	5.15
	$Hfo-wOH + Mg^{2+} \rightarrow Hfo-wOMg^+ + H^+$	4.60
exchange sites	0.6 mol sites / mol $Fe(OH)_3$	

Hfo-w denotes the weak binding sites of hydrous ferric oxides; <sup>1</sup> Fitted to measurements.

solution, the aqueous  $Fe^{3+}$  and  $Al^{3+}$  concentrations, and the sulphur content in the precipitates. The following uncertainties were assumed: starting pH,  $\pm 0.05$  units; Fe and Al concentrations,  $\pm 5\%$ ; and S content,  $\pm 20\%$ .

### Modelled Titration Curves

Modelled titration curves are shown in Figure 4. In each plot, the measured curve was plotted together with the simulated curve and the uncertainty interval associated with the analyses. The first titration curve (Figure 4A), derived with the hydroxide model, shows two plateaus. The Fe buffer sets in at  $pH \approx 3$  and the Al buffer at  $pH \approx 4.5$ . Compared to the measured curve, however, the plateaus are distinctively too long.

In addition, there is no buffering in section IV of the titration curve. Consequently, the hydroxide model is too simple to quantitatively describe the neutralisation of the lake water. The hydroxide model does not account for  $SO_4$  in the precipitating phases.

In Figure 4B, the precipitation of Fe and Al hydroxy-sulphates instead of hydroxides leads to a shortening of the Fe and Al buffer plateaus, better approximating the measured curve. The pH rise after the Al buffer, however, is still much too steep. The buffer plateau lengths are shorter because when  $SO_4$  substitutes for the hydroxide ions, less hydrogen ions are released per mole of Fe or Al (Table 1B).

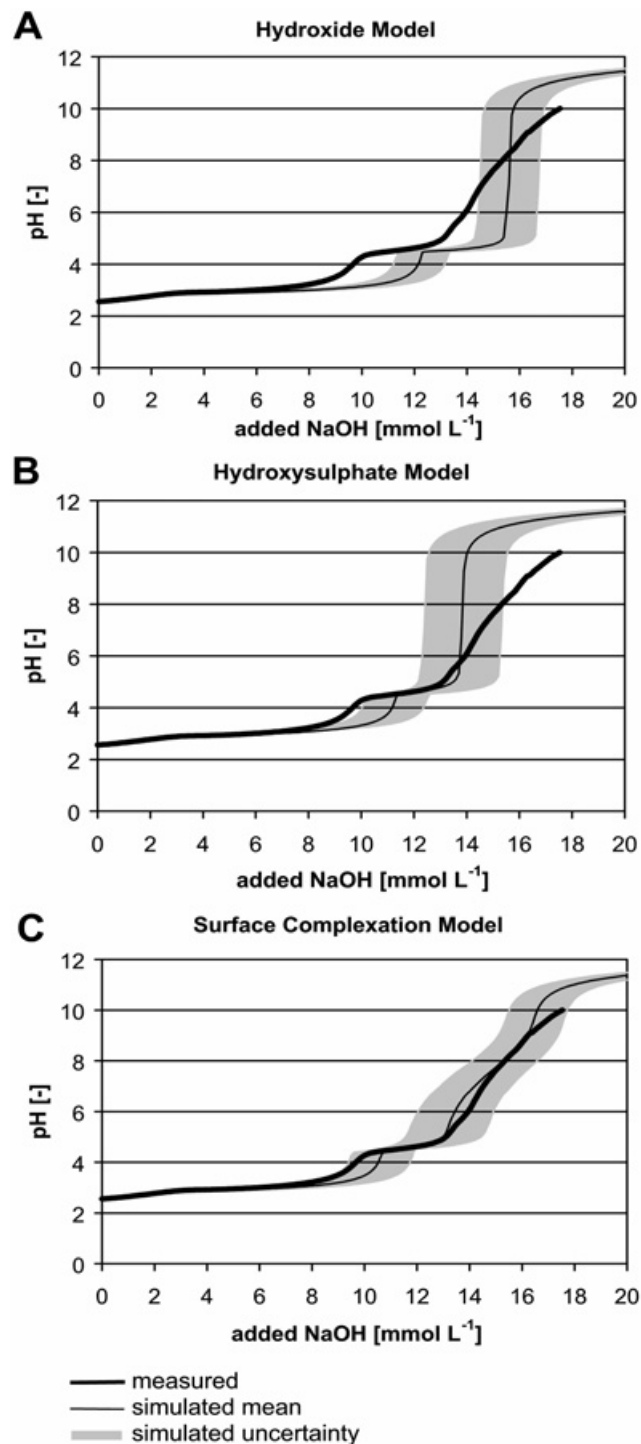
Figure 4C illustrates  $SO_4$  binding by surface complexation, which is reversible, in contrast to the



**Table 2.** Solubility products of iron and aluminium hydroxides and hydroxysulphates in the literature

Mineral	Precipitation reaction	pK <sub>sp</sub>	
Fe amorphous ferrihydrite	$\text{Fe}^{3+} + 3 \text{H}_2\text{O} \rightarrow \text{Fe}(\text{OH})_3 + 3 \text{H}^+$	4.9	[1]
schwertmannite	$8 \text{Fe}^{3+} + \text{SO}_4^{2-} + 14 \text{H}_2\text{O} \rightarrow \text{Fe}_8\text{O}_8(\text{OH})_6\text{SO}_4 + 22 \text{H}^+$	$18 \pm 2.5$	[2]
amorphous Al-hydroxide	$\text{Al}^{3+} + 3 \text{H}_2\text{O} \rightarrow \text{Al}(\text{OH})_3 + 3 \text{H}^+$	10.8	[1]
Al gibbsite	$\text{Al}^{3+} + 3 \text{H}_2\text{O} \rightarrow \text{Al}(\text{OH})_3 + 3 \text{H}^+$	8.1	[1]
basaluminite	$\text{Al}^{3+} + 0.25 \text{SO}_4^{2-} + 2.5 \text{H}_2\text{O} \rightarrow \text{Al}(\text{OH})_{2.5}(\text{SO}_4)_{0.25} + 2.5 \text{H}^+$	5.7	[1]

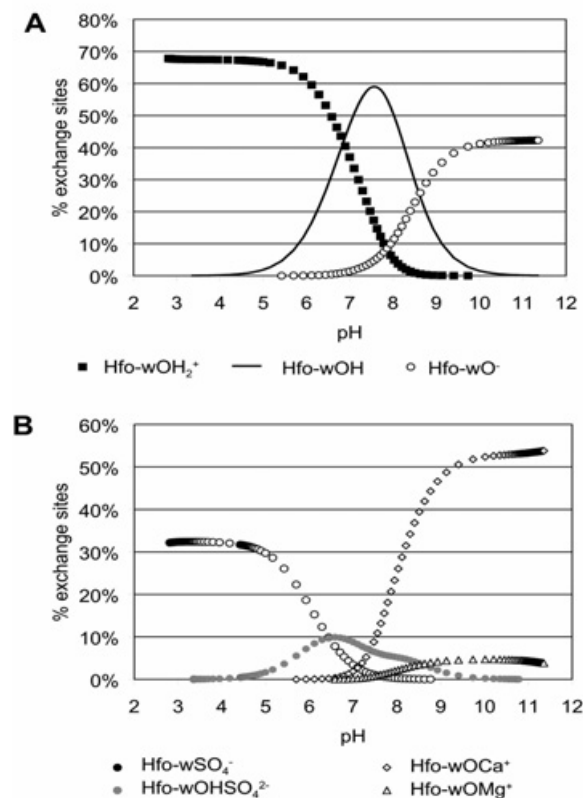
[1] Parkhurst and Appelo 1999; [2] Bigham et al. 1996



**Figure 4.** Simulated titration curves using different model assumptions with respect to solid phase reactions (see text)

hydroxysulphate model. Like the second model, the surface complexation model has shorter Fe and Al buffer plateaus than the hydroxide model, but it also shows a pronounced buffering in the last section of the titration curve, and thus best approximates the measured titration curve. The shortening of Fe and Al buffer plateaus in the model is due to  $\text{SO}_4$  and hydrogen ion adsorption in the acidic environment (Figure 5). Both processes remove hydrogen ions from the solution and therefore cause an earlier rise in pH (Table 1C). Between pH = 5 and 8,  $\text{SO}_4$  and hydrogen ions are released again from the solid phase and Ca and Mg are bound, leading to an additional buffering effect in the neutral pH range.

Titration curves were recorded under continuous stirring, i.e. in an open system. However, there was no equilibrium between the solution and the



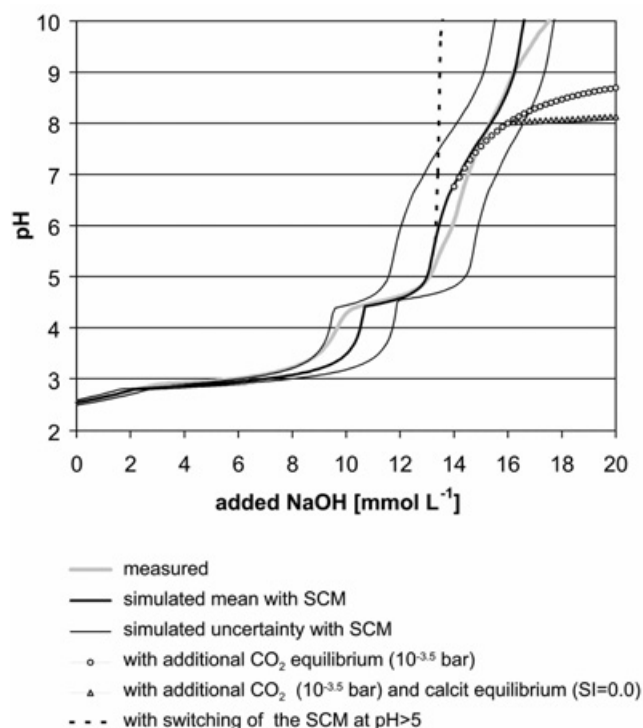
**Figure 5.** Distribution of species on the surface of iron hydroxide at varied pH values using the surface complexation model and standard parameterisation given in Table 1. (Hfo-w denotes the weak binding sites on the hydrous ferric oxide surface.)

atmosphere with respect to CO<sub>2</sub>. According to the model calculations, equilibrium with the atmosphere with respect to CO<sub>2</sub> would lead to the formation of carbonic acid buffering at pH > 7 and even to the precipitation of calcium carbonate at pH > 8 (Figure 6). The carbonic acid /carbonate buffer, however, was not observed in the titration experiments. This indicates that CO<sub>2</sub> delivery is limited in the laboratory experiments at the time scale of a few hours to a few days. Therefore, CO<sub>2</sub> was neglected in the model calculations. This simplification, though, only applies to the laboratory experiments and not to the field.

Experiments and model calculations demonstrate the important role of SO<sub>4</sub> in the precipitates. SO<sub>4</sub> leads to a shortening of the Fe and Al buffer plateaus. Only by taking SO<sub>4</sub> in the precipitates into account is it possible to explain the lengths of the measured buffer plateaus. Concerning the type of SO<sub>4</sub> binding, some questions remain unresolved. Phase analyses point to the fact that the precipitating phases are iron hydroxysulphate (schwertmannite) and aluminium hydroxysulphate in the acidic environment. On the other hand, a comparison of the acidic precipitate at pH = 5.0 with the alkaline precipitate at pH = 8.5 (Figure 3) shows that SO<sub>4</sub> is released from the solid phase during titration and that Ca and Mg are bound. This observation favours surface binding.

Combining both suggests that iron and aluminium hydroxysulphates precipitate in the acidic environment and are then transformed to hydroxides or hydrooxides during the titration, whereby the previously bound SO<sub>4</sub> is released. Such a mineral transformation is known to take place during the ageing of schwertmannite (Bigham et al. 1996). Considering the overall chemistry with respect to buffering, both mineral transformation (Equation 1) and SO<sub>4</sub> desorption (Equation 2) release hydrogen ions. Together with the adsorption of Ca and Mg, these act as additional buffering mechanisms in the neutral pH range.

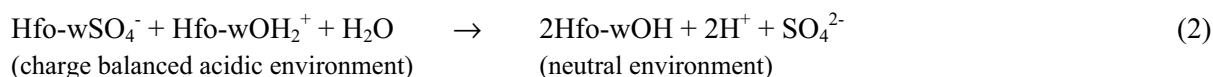
The transformation from schwertmannite to goethite is a kinetically controlled process. In a strongly acidic environment, the mineral transformation is a long-lasting process, taking years (Bigham et al. 1996). We do not know how much time it takes in the weakly acidic and neutral environment. In contrast to mineral transformation, surface complexation can be approximated as an equilibrium process. As the titration experiments did not show any substantial



**Figure 6.** Comparison of different chemical models for the buffering at pH > 5. (SCM denotes the surface complexation model for iron hydroxide.)

time dependency, we favour the concept of surface complexation for a model-based description of buffering mechanisms.

The conservative balance of the ion-specific acidity accounting for complex compounds (e.g. hydroxy complexes) and activity coefficients (Table 3) results in approximately the same alkalinity demand for neutralisation up to pH = 8.2 as does the model-based balance of the acidity considering solid-bound SO<sub>4</sub> and surface exchange processes (Table 4). However, the course of buffering is different (Figure 7), which is important in the context of controlling the processes in the field. Surface complexation of free hydrogen ions and SO<sub>4</sub> ions on iron hydroxides leads to a maximum shortening of approximately 1.5 meq L<sup>-1</sup> of the Fe buffer plateau. The process is obviously reversible if the sediment remains in the system. At increasing pH up to approximately 8, this shortening of the buffer plateau is almost completely compensated by desorption of SO<sub>4</sub>. The precipitation of aluminium hydroxysulphate terminates at pH ≈ 5.5. SO<sub>4</sub> binding leads to a shortening of the Al buffer plateau of approximately 0.8 meq L<sup>-1</sup>. In addition to SO<sub>4</sub> desorption, at pH > 7, deprotonation of iron hydroxides and the surface complexation of Ca and Mg on iron hydroxides,



**Table 3.** Conservative values of buffering

Parameter	Produced Acidity	pH Range of Buffering
Hydrogen ion <sup>1</sup>	3.2 meq L <sup>-1</sup>	2.55...4.3
Hydrogen sulphate	1.3 meq L <sup>-1</sup>	2.55...4.3
Iron(III) <sup>2</sup>	7.7 meq L <sup>-1</sup>	2.55...3.5
Aluminium <sup>2</sup>	3.2 meq L <sup>-1</sup>	4.5...5.5
Carbonic acid	< 0.1 meq L <sup>-1</sup>	4.3...8.2
Sum	15.4 meq L <sup>-1</sup>	2.55...8.2

<sup>1</sup>Considering the ion activity coefficient; <sup>2</sup> considering the hydroxy complexes at pH = 2.55

increase buffering. Up to pH  $\approx$  8.2, there is an additional alkalinity demand of approximately 0.7 meq L<sup>-1</sup>.

We assume that aluminium hydroxides exhibit the same properties as iron hydroxides with respect to surface complexation. However, thermodynamic data are not available for surface complexation on aluminium hydroxides. This mainly affects titration curves in the neutral and alkaline range (pH > 6) and may lead to an underestimation of the surface complexation buffer in the model. The buffer intensity is defined as the degree to which pH changes when alkalinity is added (Stumm and Morgan 1996):

$$\beta = -d(\text{pH})/d\text{Alk}_{\text{add}}$$

Figure 8 depicts the measured and modelled buffer intensity, which agree well up to pH  $\approx$  9.

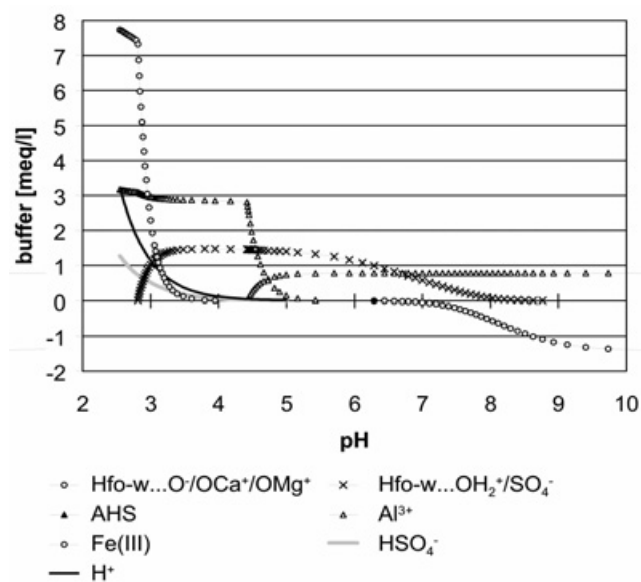
## Conclusions

The experimental results and model calculations on the acidic lake water lead to several conclusions. First, the titration curve can be divided into four sections: (1) the neutralisation of free hydrogen ions and hydrogen sulphate deprotonation; (2) homogeneous and heterogeneous Fe<sup>3+</sup> buffering with SO<sub>4</sub> binding; (3) homogeneous and heterogeneous Al buffering with SO<sub>4</sub> binding and; (4) buffering by surface exchange processes. Buffering by carbonic acid was not a factor.

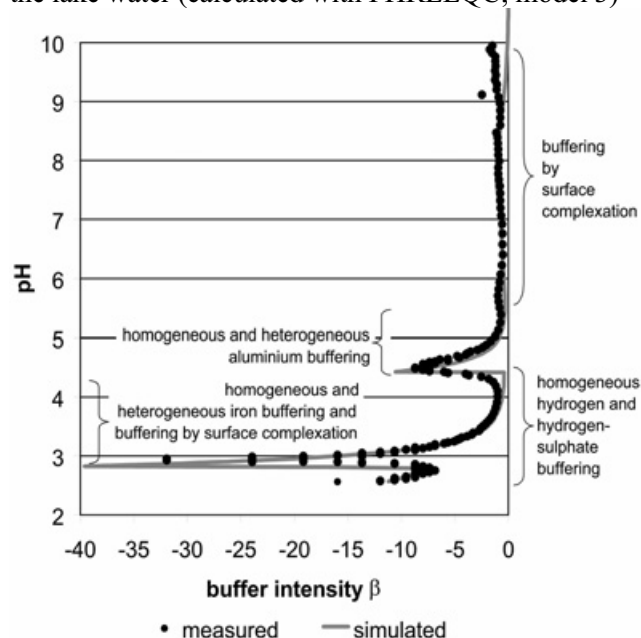
Second, SO<sub>4</sub> that co-precipitates with the Fe and Al mineral phases distinctively shortens the buffer plateaus in the acidic range.

Third, at pH > 5, buffering processes occur that are based on surface effects of the precipitating phases. These lead to a damped increase of the titration curve.

Finally, a phase model consisting of ferrihydrite, aluminium hydroxysulphate, and manganese oxide with surface complexation of SO<sub>4</sub>, Ca, and Mg on the ferrihydrite surface proved to be suitable for a quantitative description of the measured titration curve, indicating that surface complexation on fresh



**Figure 7.** pH-dependent concentrations of acidity and alkalinity bearing components, and surface reactions in the lake water (calculated with PHREEQC; model 3)



**Figure 8.** Buffer intensity of the buffering processes for the measured and the simulated titration curve.

precipitates plays an important role during the neutralisation of acidic mining lake water.

## Acknowledgements

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**Table 4.** Buffering values, considering surface complexation and aluminium hydroxysulphate precipitation

Parameter	Produced Acidity	Consumed Acidity	pH Range of Buffering
Hydrogen ion <sup>1</sup>	3.2 meq L <sup>-1</sup>		2.55...4.3
Hydrogen sulphate	1.3 meq L <sup>-1</sup>		2.55...4.3
Iron(III) <sup>2</sup>	7.7 meq L <sup>-1</sup>		2.55...3.5
Hfo-w...OH <sub>2</sub> <sup>+</sup> /SO <sub>4</sub> <sup>-</sup>		-1.5 meq L <sup>-1</sup>	2.8...3.8
Aluminium <sup>2</sup>	3.2 meq L <sup>-1</sup>		4.5...5.5
AHS		-0.8 meq L <sup>-1</sup>	4.5...5.5
Hfo-w...OH <sub>2</sub> <sup>+</sup> /SO <sub>4</sub> <sup>-</sup>	1.5 meq L <sup>-1</sup>		3.8...8.2
Carbonic acid	<0.1 meq L <sup>-1</sup>		4.3...8.2
Hfo-w...O <sup>-</sup> /OCa <sup>+</sup> /OMg <sup>+</sup>	0.7 meq L <sup>-1</sup>		6.5...8.2
Sum	15.3 meq L <sup>-1</sup>		2.55...8.2

<sup>1</sup> Considering the ion activity coefficient; <sup>2</sup> considering the hydroxy complexes at pH = 2.55

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